

We claim:

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1. A gas-phase fluidized-bed reactor for polymerizing ethylenically unsaturated monomers, comprising a reactor space (1) in the form of a vertical tube, a calming zone (2) adjoining the upper part of the reactor space, a circulated gas line (3), a circulated gas compressor (4), a cooling apparatus (5), a gas distributor plate (6) which forms the lower boundary of the reactor space and, if desired, a flow divider (7), wherein the gas distributor plate (6) has a plurality of gas flow orifices (8) whose outlet sides are widened conically.
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2. A gas-phase fluidized-bed reactor as claimed in claim 1, wherein the conical widening of the gas flow orifices has an angle  $\alpha$  of from 20 to 40°.
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3. A gas-phase fluidized-bed reactor as claimed in claim 1 or 2, wherein the remaining planar part of the upper side of the gas distributor plate is less than 10% of the total area of the gas distributor plate.
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4. A gas-phase fluidized-bed reactor as claimed in any of claims 1 to 3, wherein the gas flow orifices of the gas distributor plate are configured such that the pressure drop on flowing through the bottom plate is at least 30% of the pressure drop experienced by the gas mixture on flowing through the fluidized bed.
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5. A gas-phase fluidized-bed reactor as claimed in any of claims 1 to 4, wherein the diameter of the gas flow orifices is from 2 to 5 mm at their narrowest point.
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6. A gas-phase fluidized-bed reactor as claimed in any of claims 1 to 5, wherein a flow divider (7) is installed below the gas distributor plate.
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7. A gas distributor plate (6) as set forth in any of claims 1 to 5.

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8. A process for polymerizing ethylene or for copolymerizing ethylene with C<sub>3</sub>-C<sub>8</sub>- $\alpha$ -olefins at from 30 to 125°C and a pressure of from 10 to 90 bar, wherein the process is carried out in a gas-phase fluidized-bed reactor as claimed in any of claims 1 to 6.

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9. A process as claimed in claim 8, wherein the polymerization is carried out in the presence of condensed monomers.

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